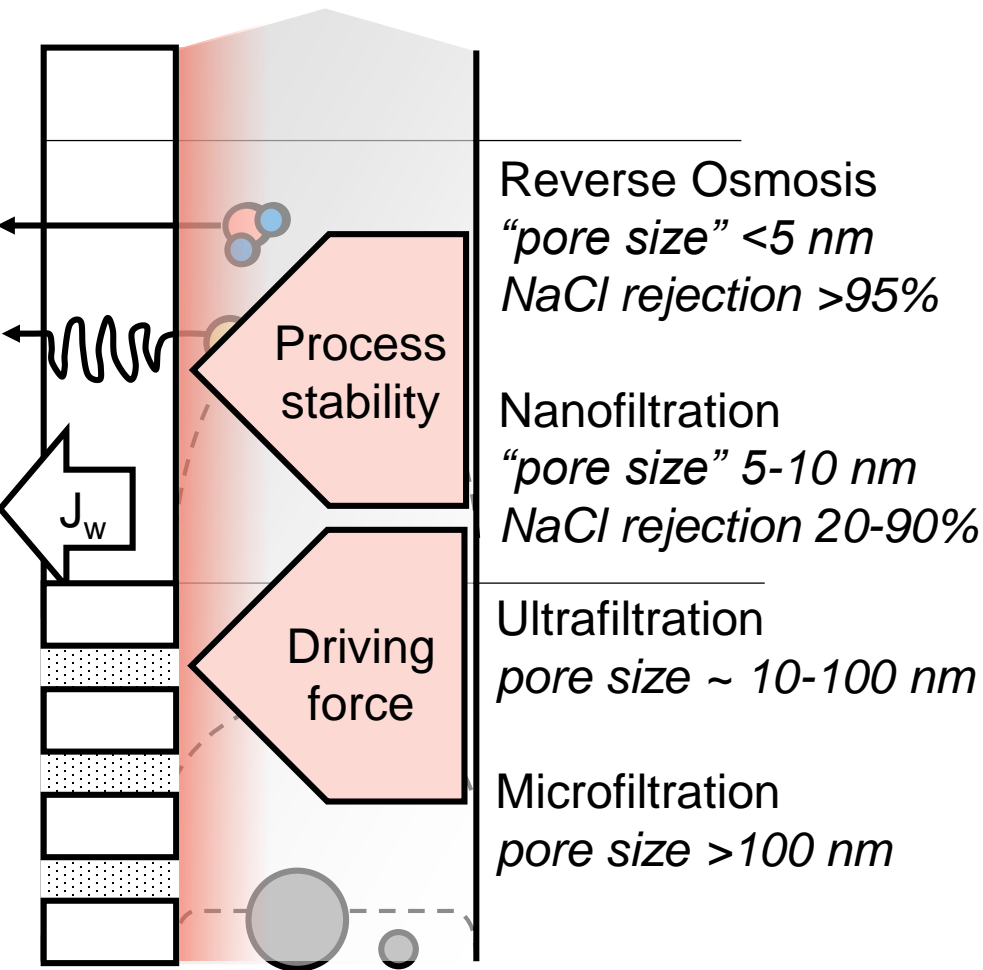


# Manipulation and characterization of interfacial phenomena in membrane processes

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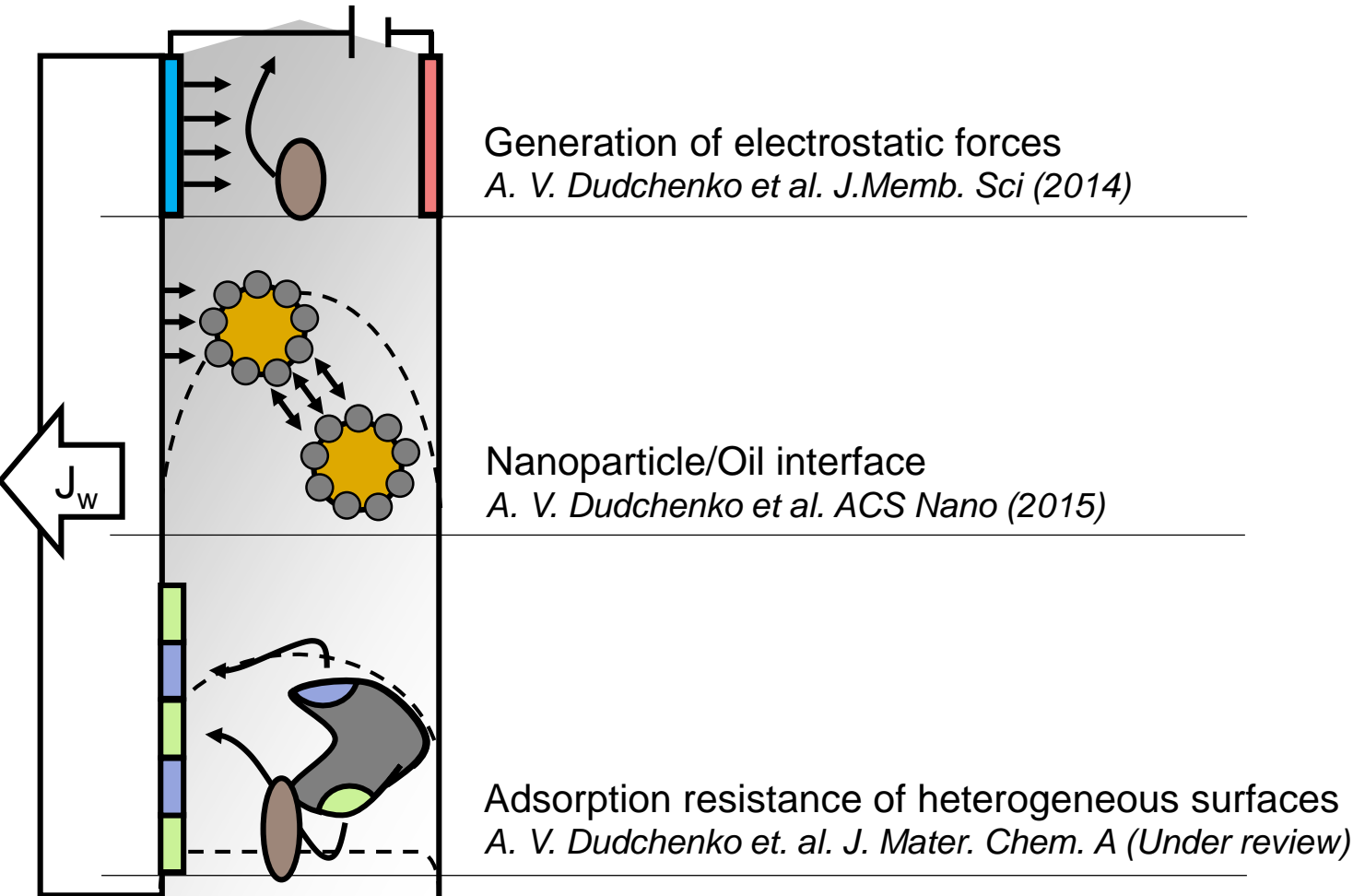
Alexander V. Dudchenko  
Department of Civil and Environmental Engineering  
Stanford University  
adudchen@stanford.edu

# Interfacial phenomena govern membrane process performance



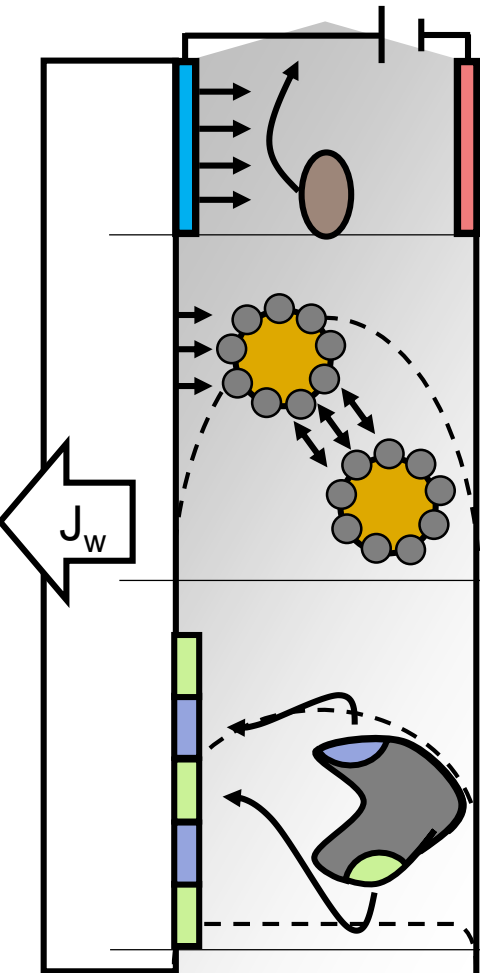
# Interfacial phenomena govern membrane process performance

## *Foulant adsorption*

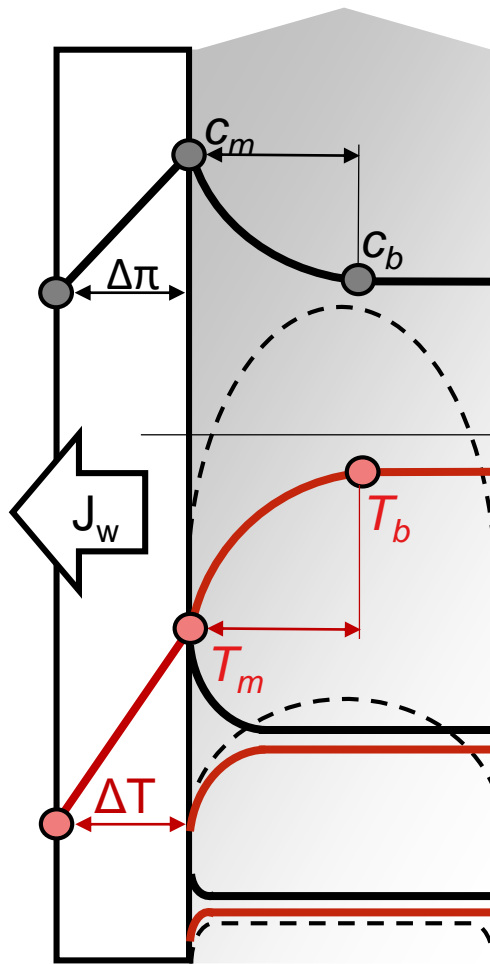


# Mass and heat transfer limits membrane process performance

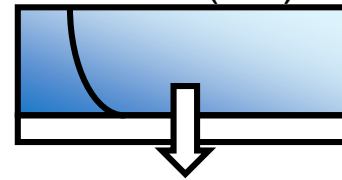
*Foulant adsorption*



*Mass and heat transfer*

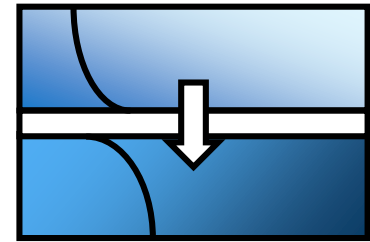


Pressure driven ( $\Delta P$ )



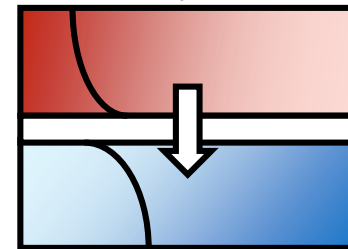
MF/UF  
NF/RO

Osmotically driven ( $\Delta \pi$ )



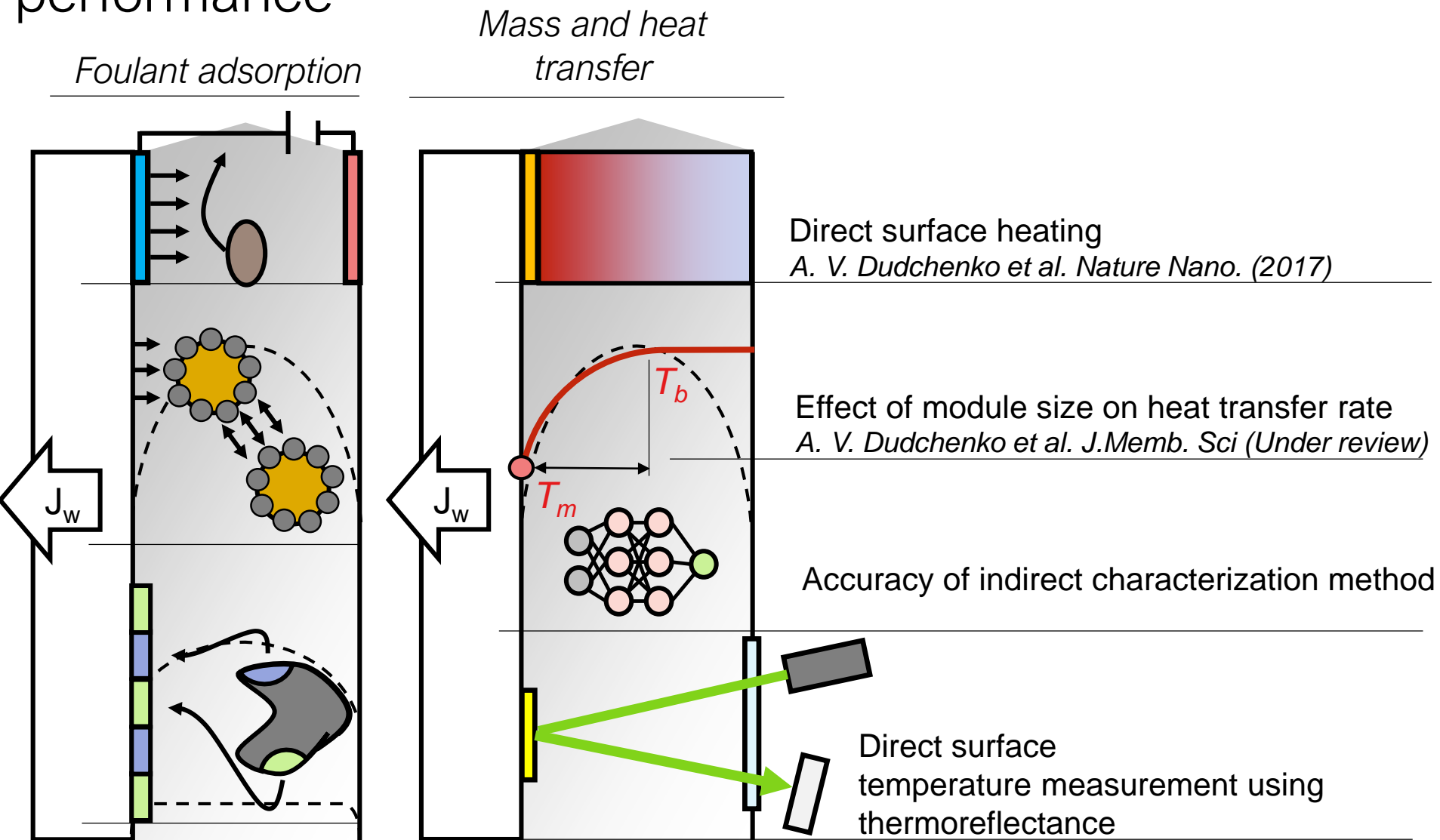
FO/PRO  
OARO

Thermally driven ( $\Delta T$ )

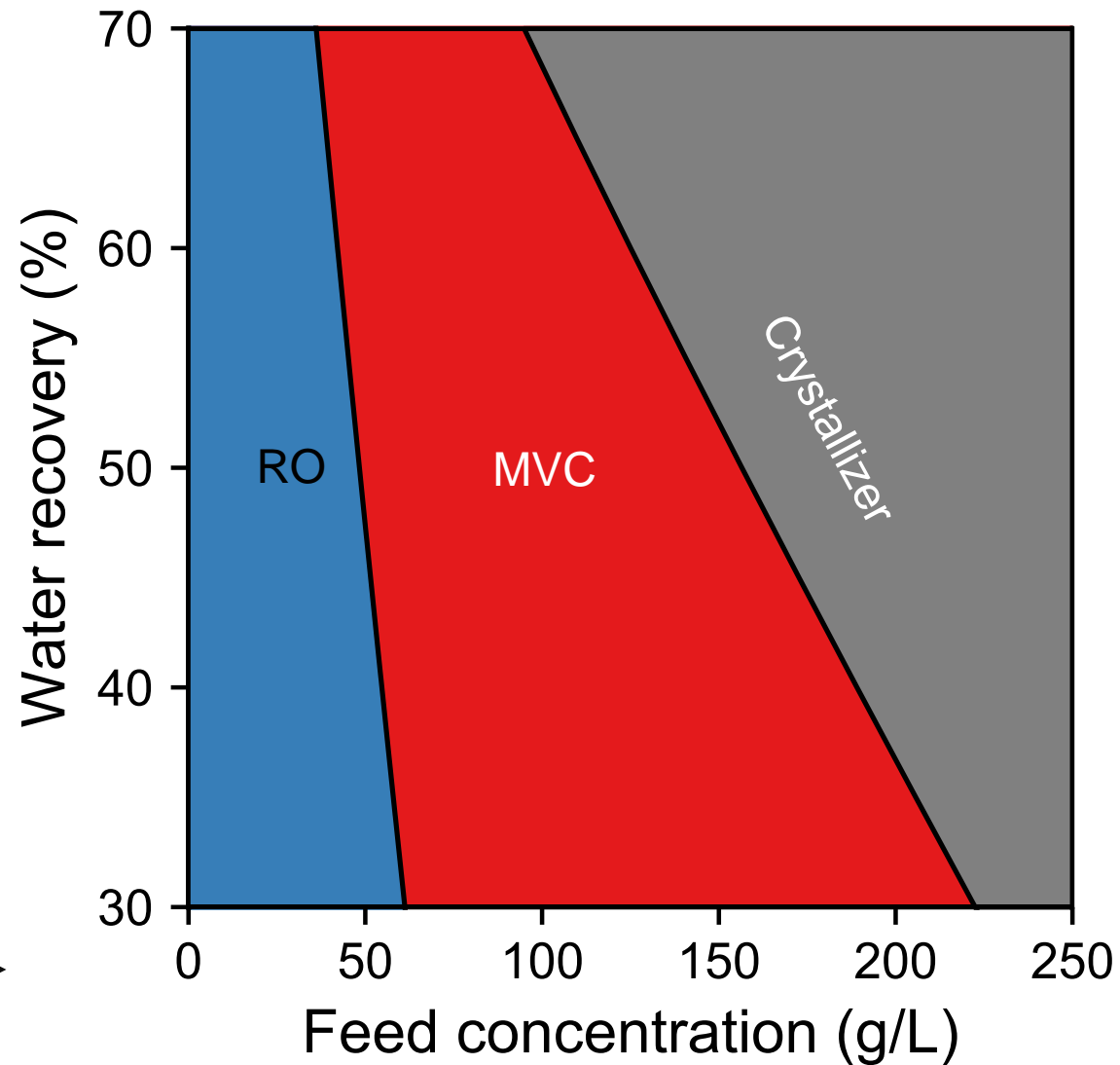
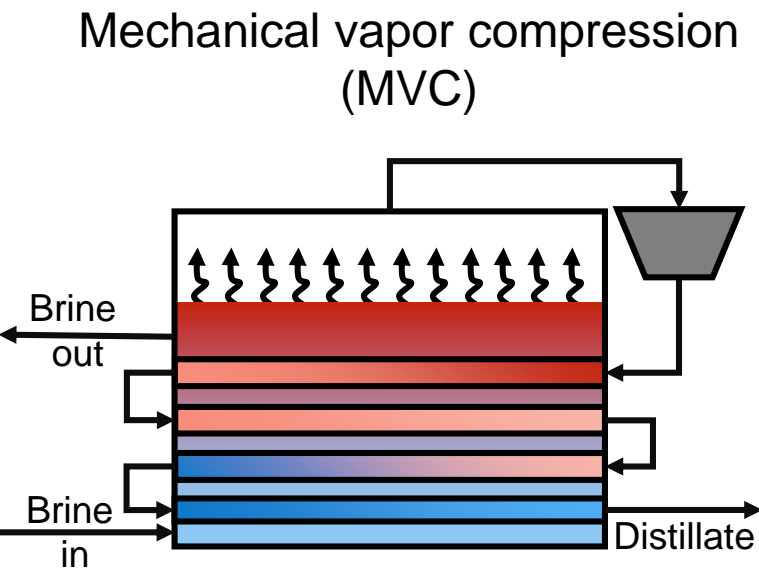
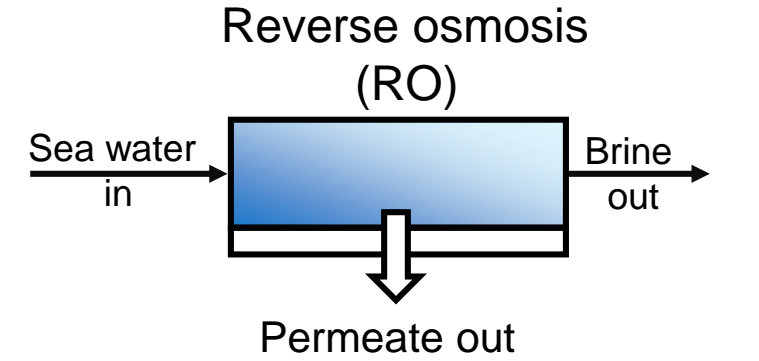


Membrane  
Distillation (MD)  
Pervaporation

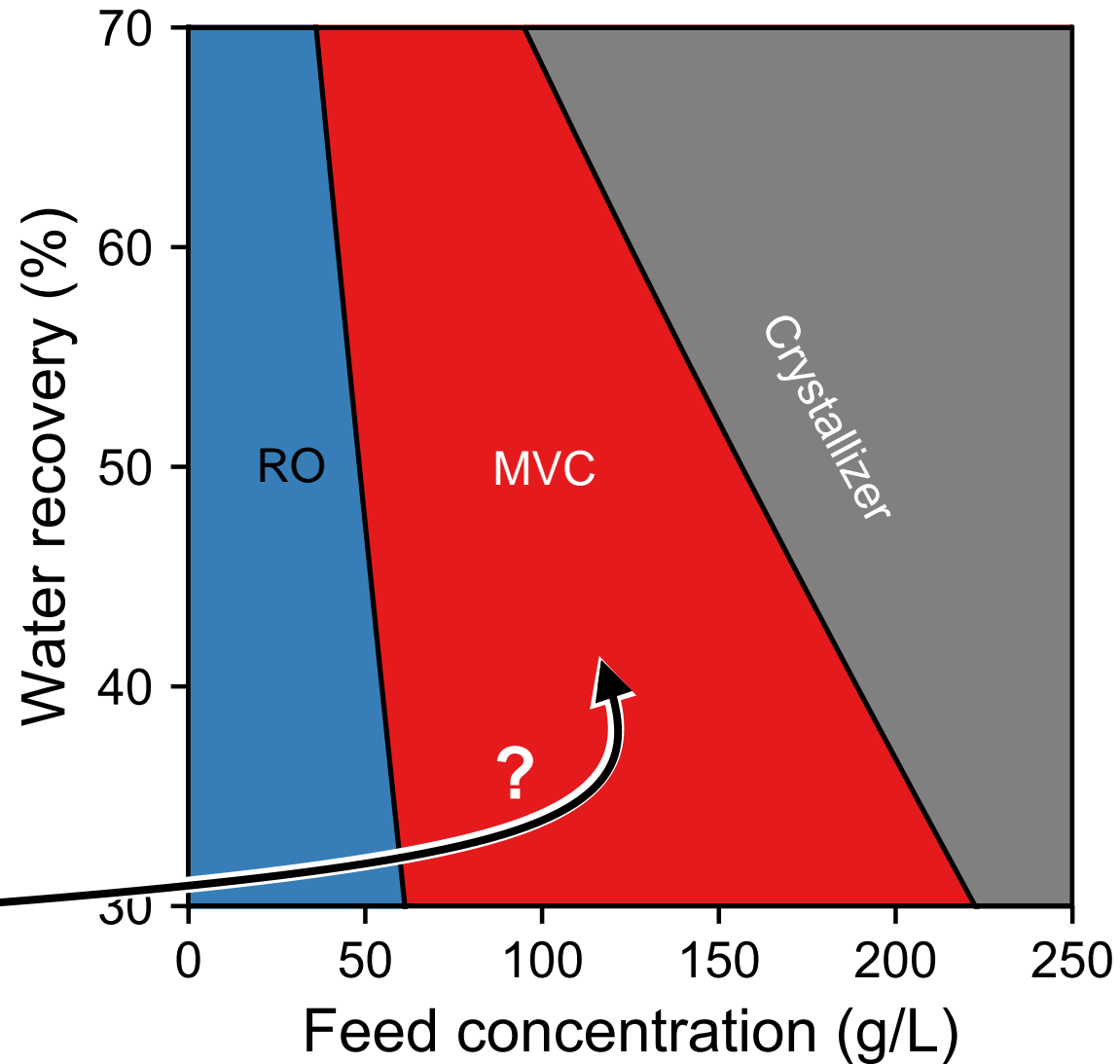
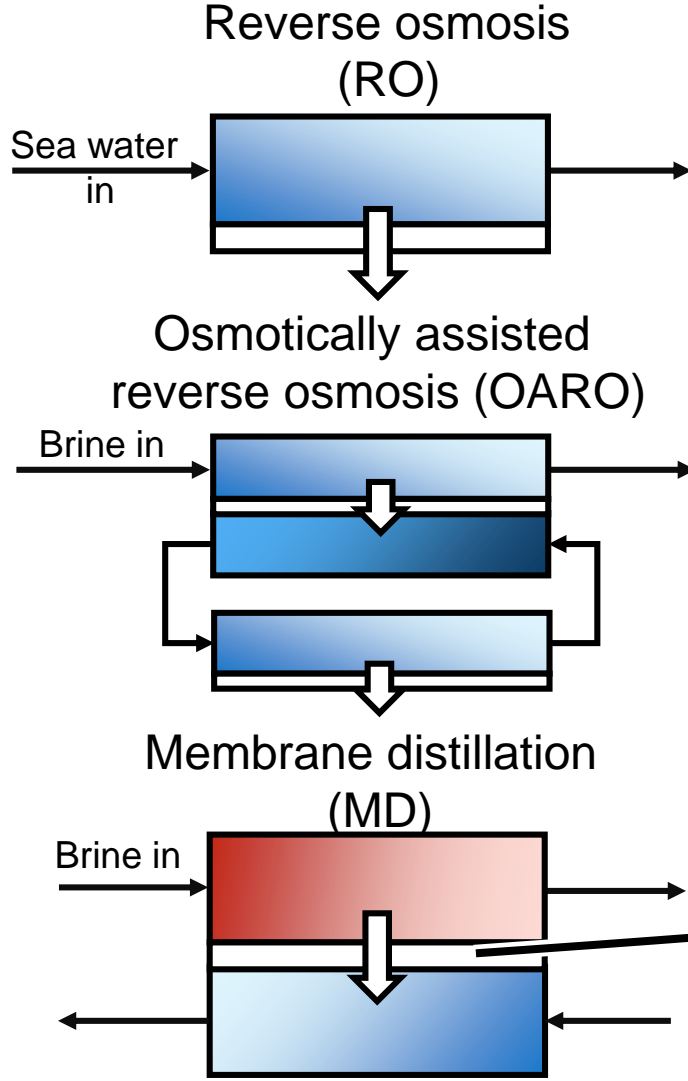
# Mass and heat transfer limits membrane process performance



# Thermal processes are current state of the art for high salinity treatment

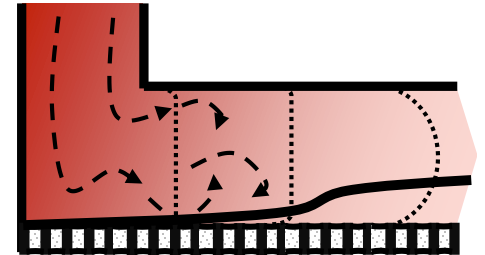


# Membrane processes can potentially displace traditional treatment processes



# Quantifying interfacial phenomena in MD

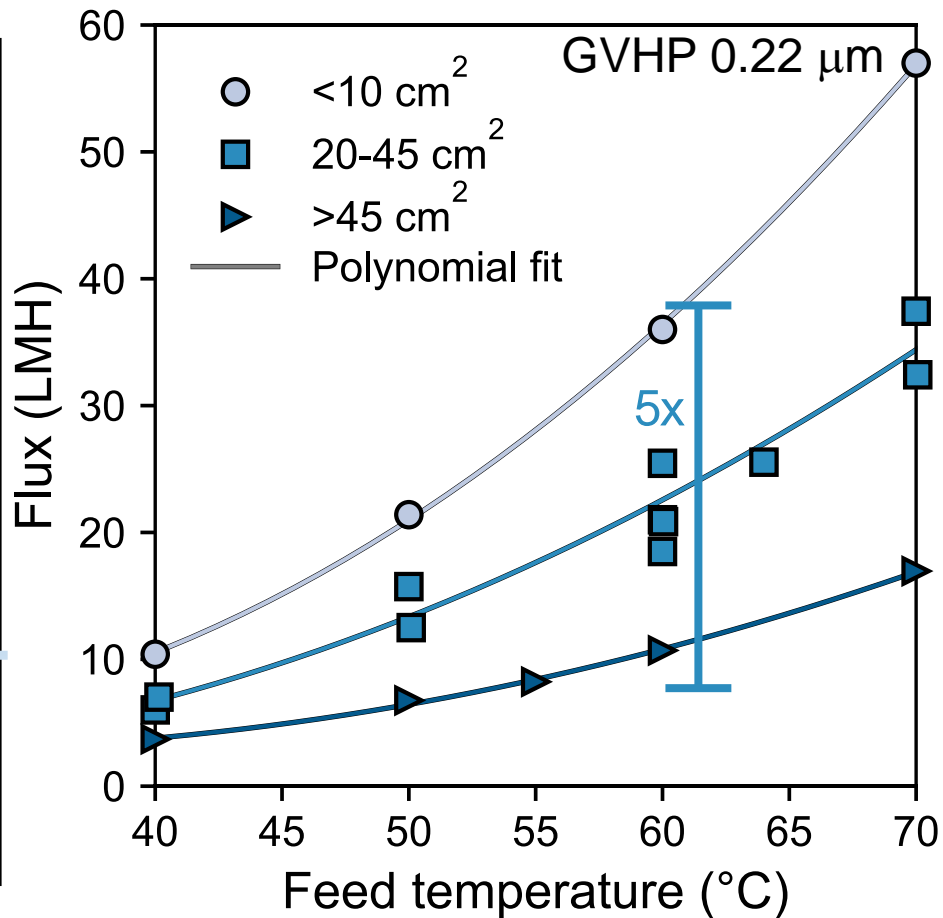
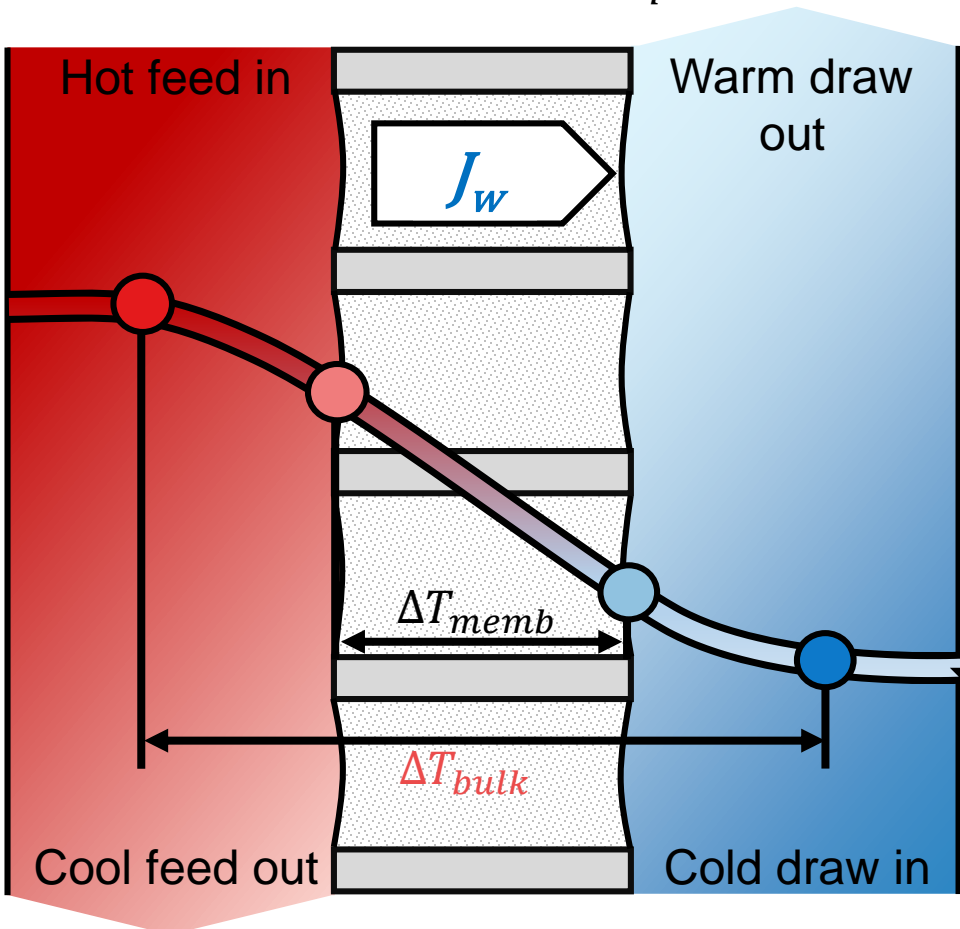
Effect of module design on heat transfer rate in MD



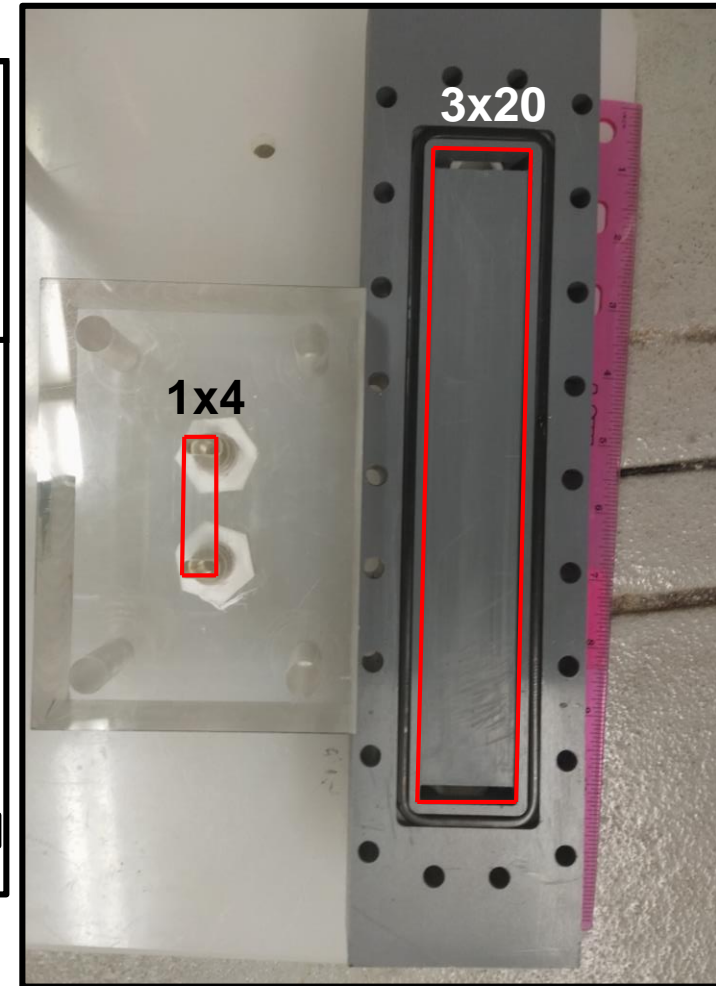
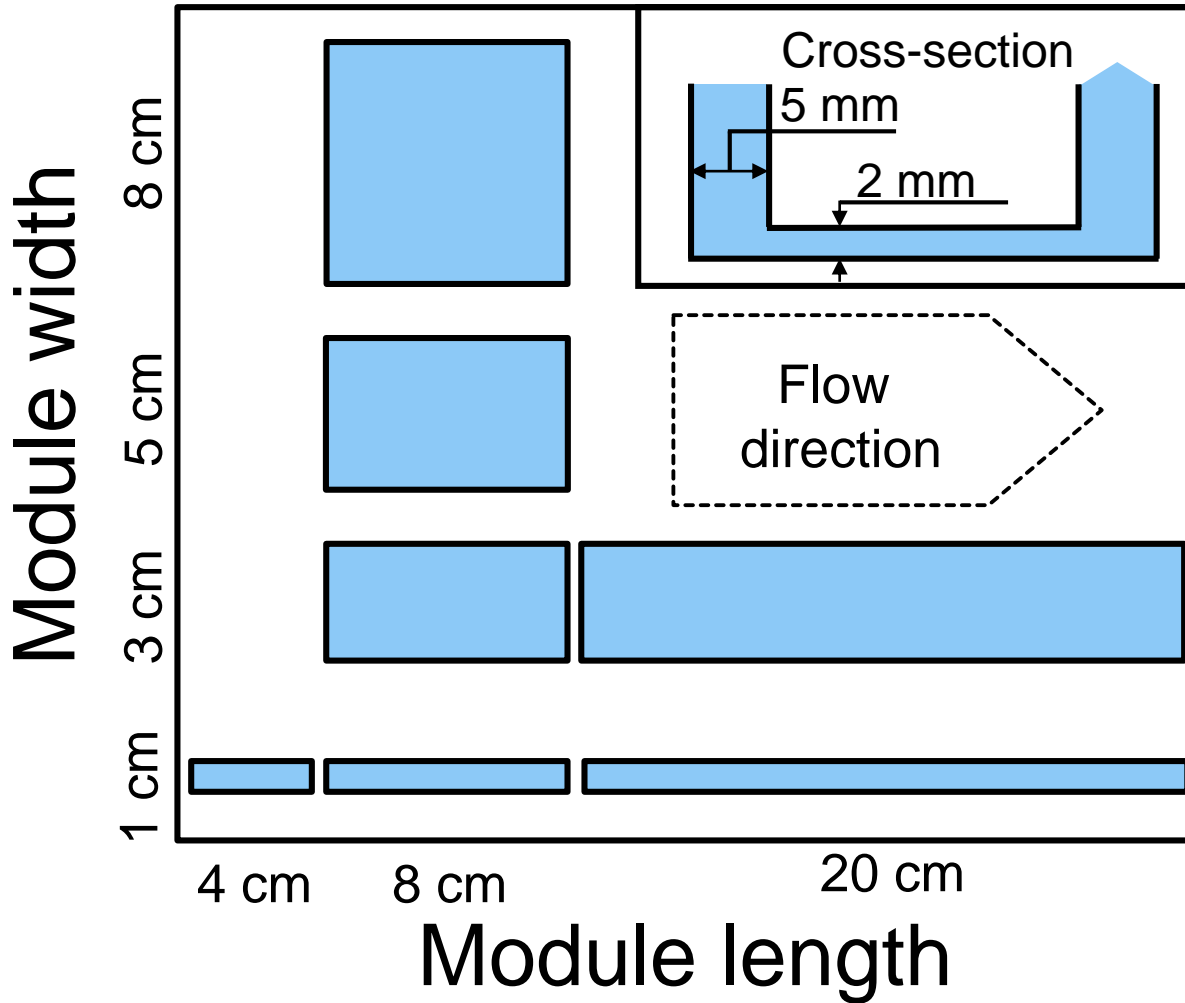


Literature data on MD reports x5 spread in permeate flux for the same membrane

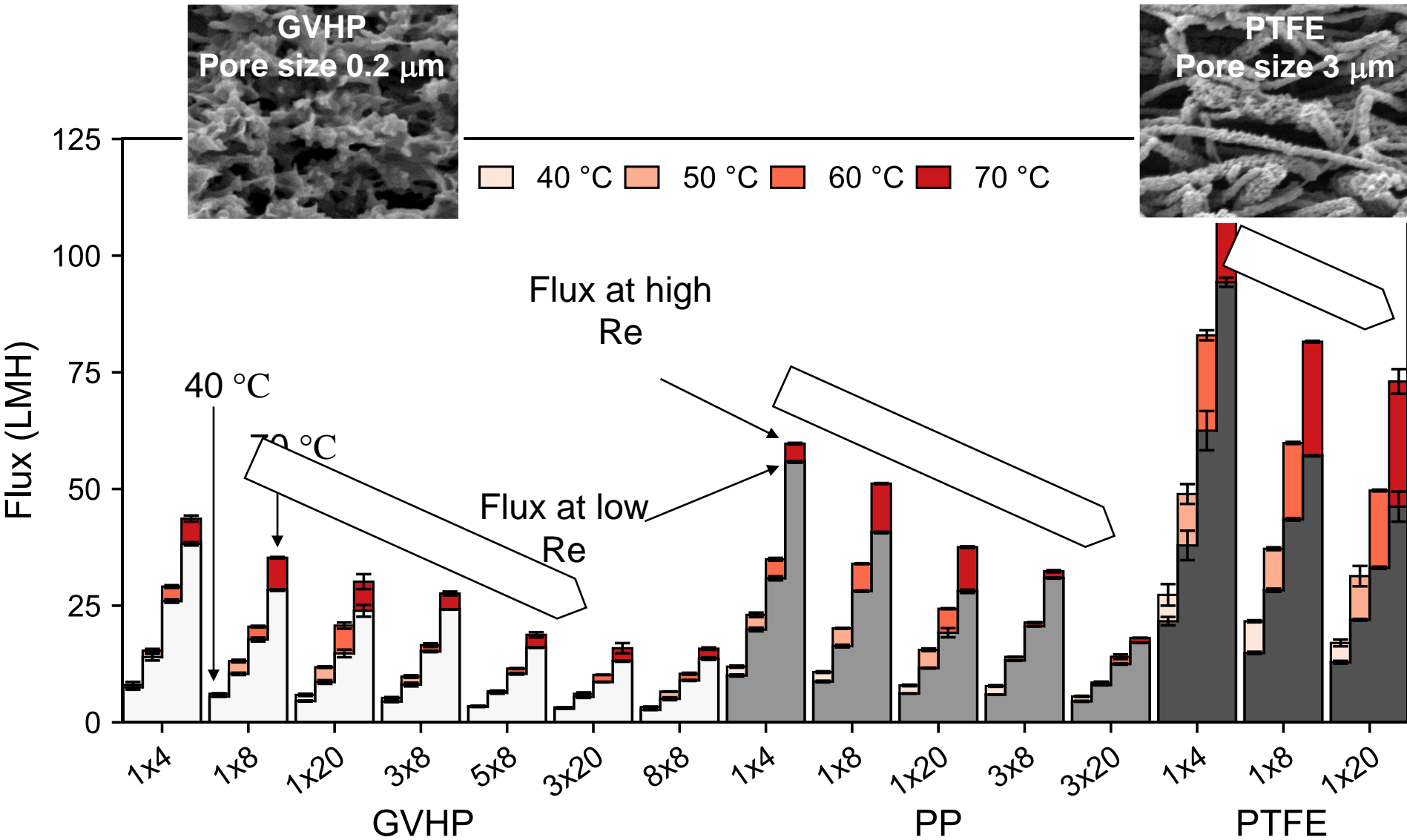
$$\text{Permeability } (\beta_{w,i}) = \frac{J_w \delta_m}{\Delta p_{vap}} \quad \Delta p_{vap} = f(\Delta T_{memb}) \quad Nu = a Re^b Pr^c \left( \frac{d_h}{L} \right)^d$$



# Effect of module dimensions tested by systematically varying module width and length

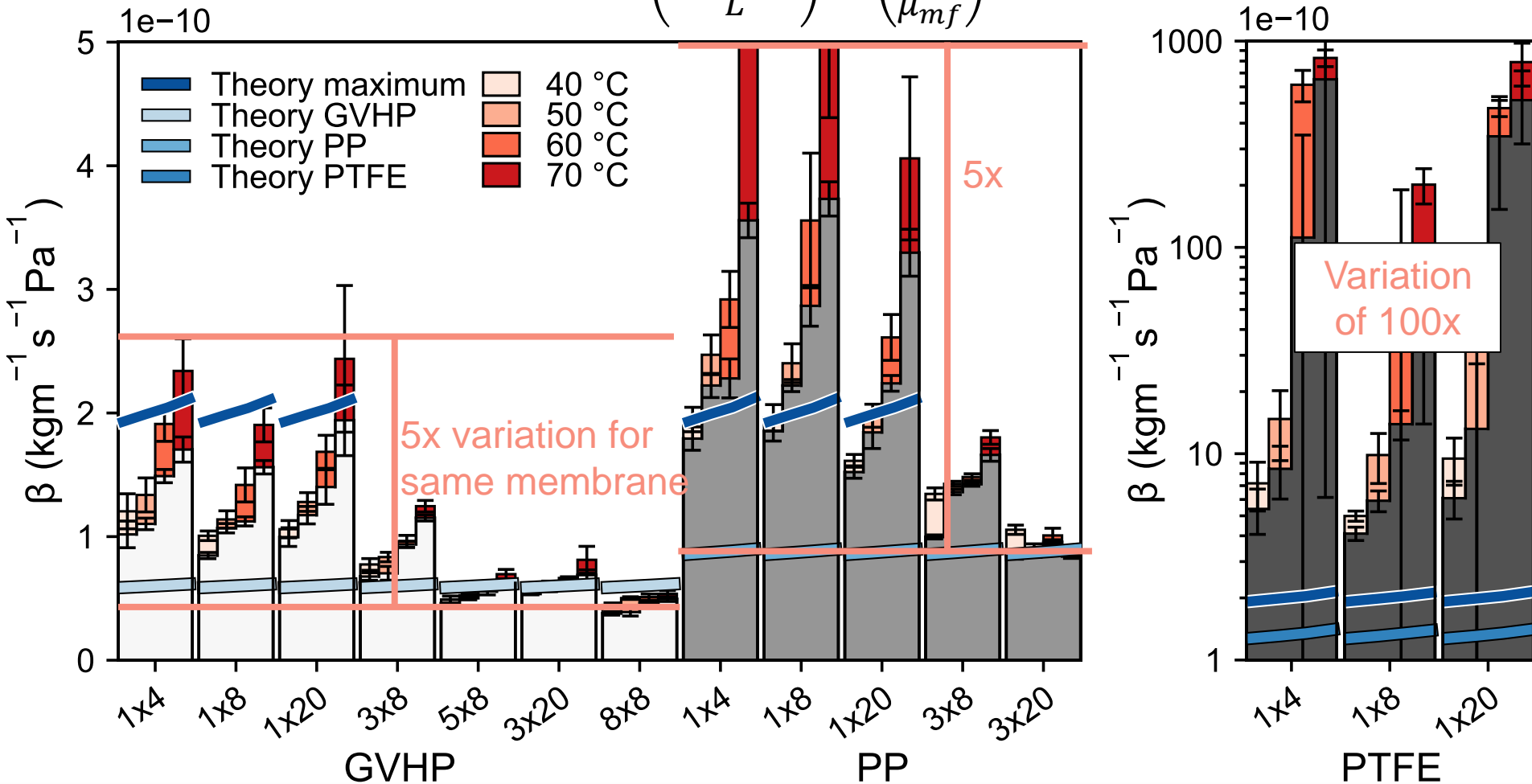


# Module area strongly impacts measured permeate flux



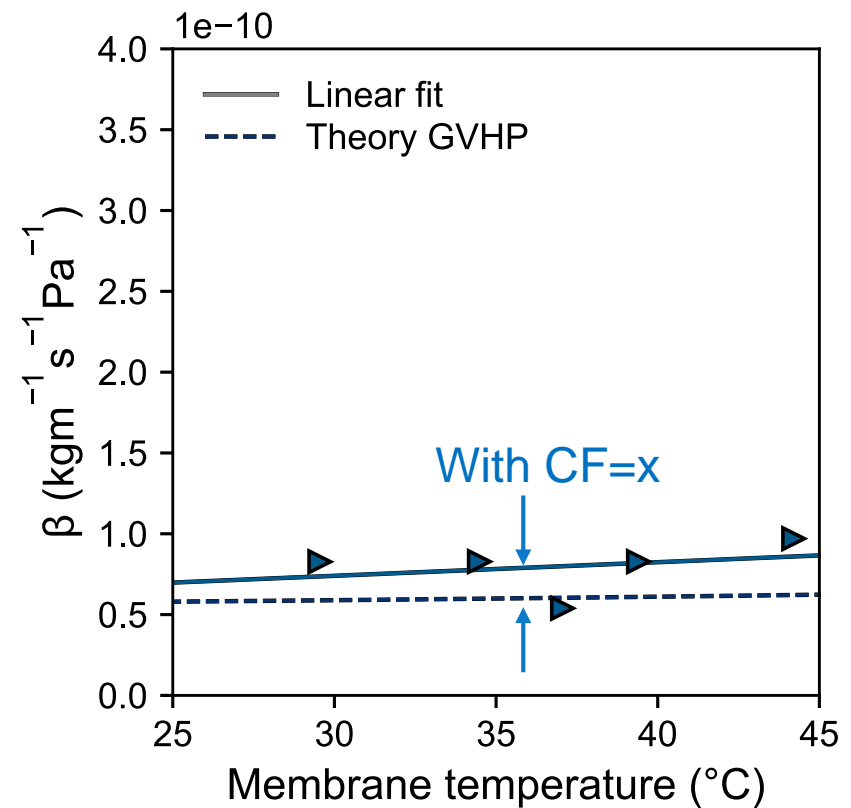
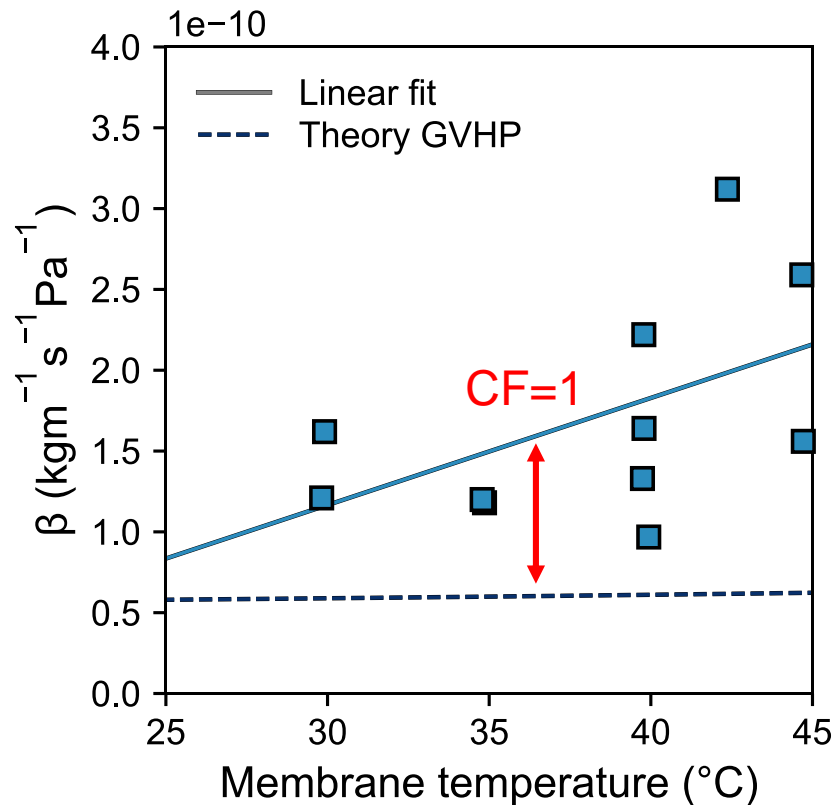
Nusselt correlations can fail to capture heat transfer in smaller modules, overestimating permeability

$$\overline{Nu} = 1.86 \left( \frac{RePrd_h}{L} \right)^{1/3} \left( \frac{\mu_{bf}}{\mu_{mf}} \right)^{0.14}$$



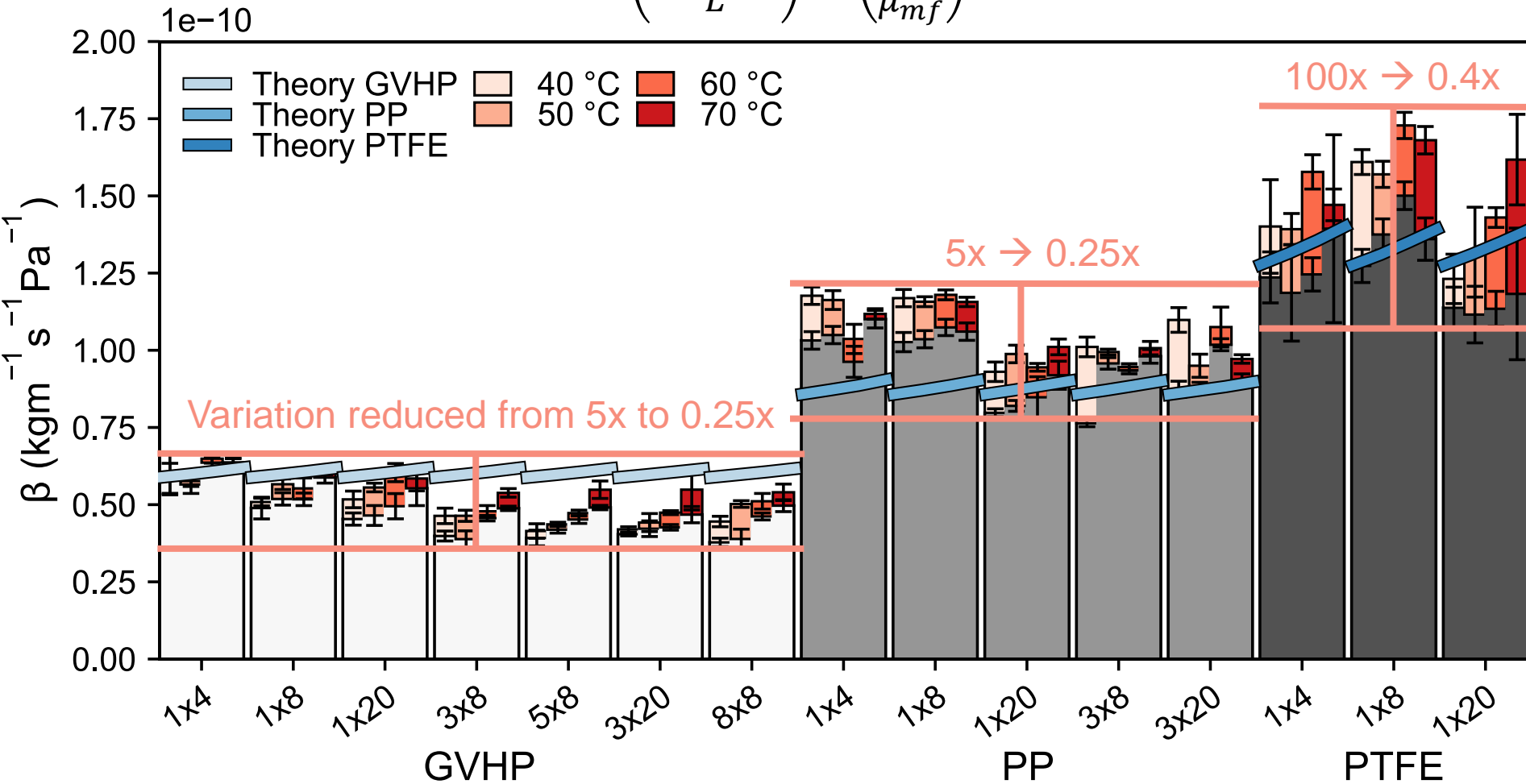
# Heat transfer rate can be validated by comparing the experimental slope to theoretical slope

$$\overline{Nu} = 1.86 \left( \frac{RePrd_h}{L} \right)^{1/3} \left( \frac{\mu_{bf}}{\mu_{mf}} \right)^{0.14} * CF$$



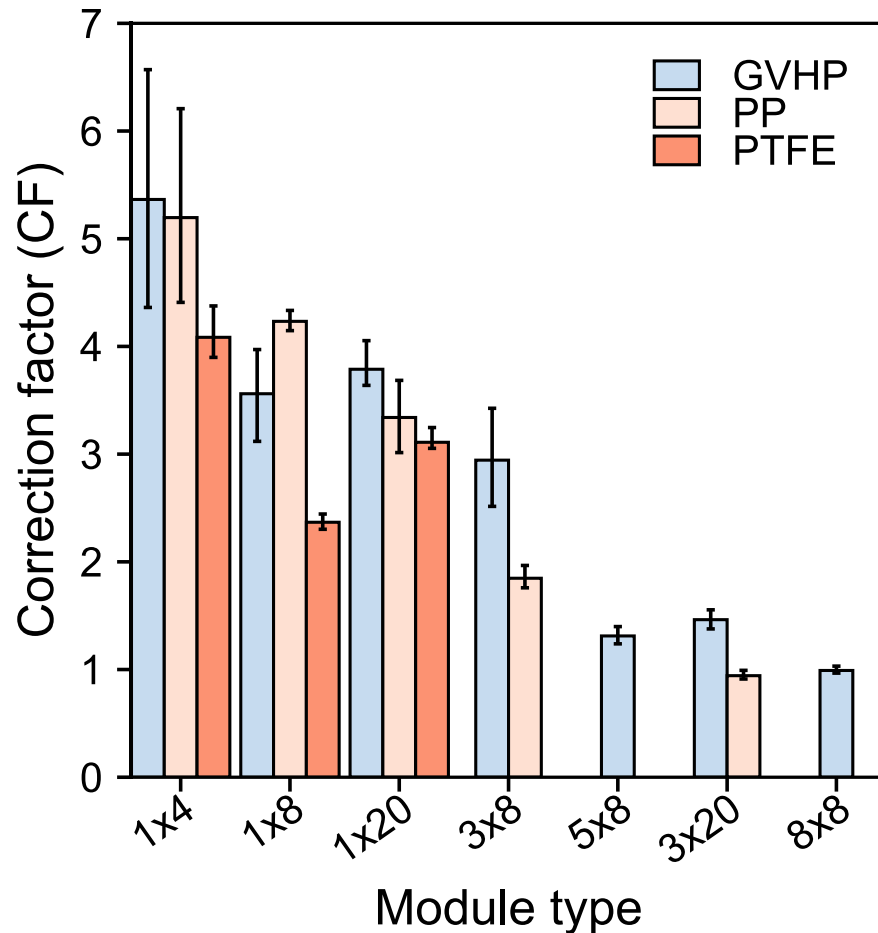
# Correction of Nusselt correlation reduces spread in permeability estimates

$$\overline{Nu} = 1.86 \left( \frac{RePrd_h}{L} \right)^{1/3} \left( \frac{\mu_{bf}}{\mu_{mf}} \right)^{0.14} \quad * \text{ CF}$$

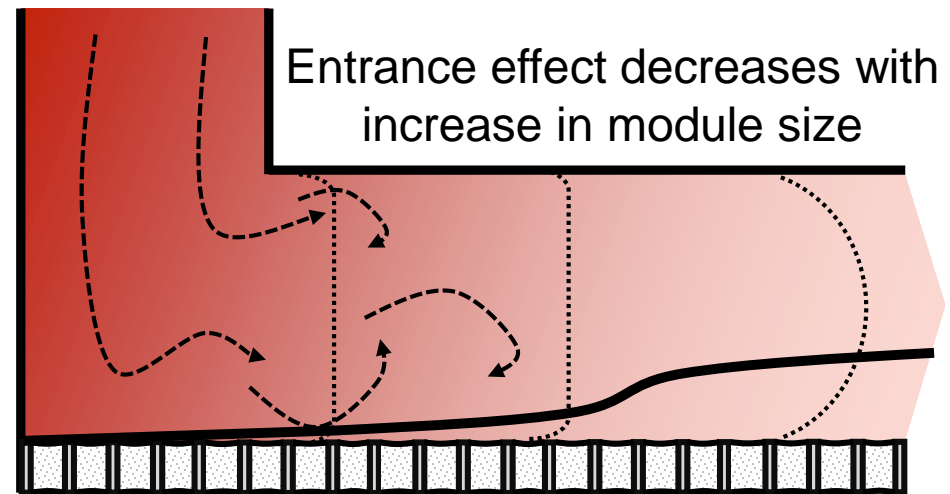
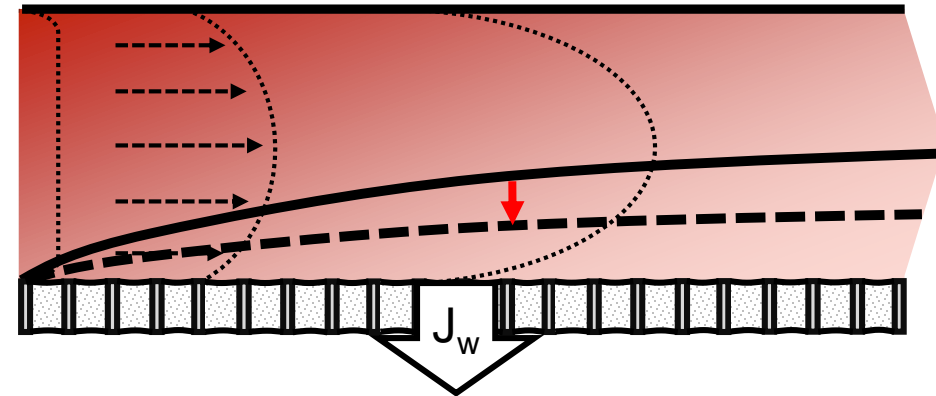


# Heat transfer in short modules is dominated by entrance effect

$$\overline{Nu} = 1.86 \left( \frac{RePrd_h}{L} \right)^{1/3} \left( \frac{\mu_{bf}}{\mu_{mf}} \right)^{0.14} * CF$$



Mass transfer effect is not observed  
(No correlation between CF and membrane type)



Comparison of experimental to theoretical trendlines provides insight into MD heat transfer rates

The slope of permeability can be used to correct existing heat transfer correlation

The entrance changes the fluid flow in the module

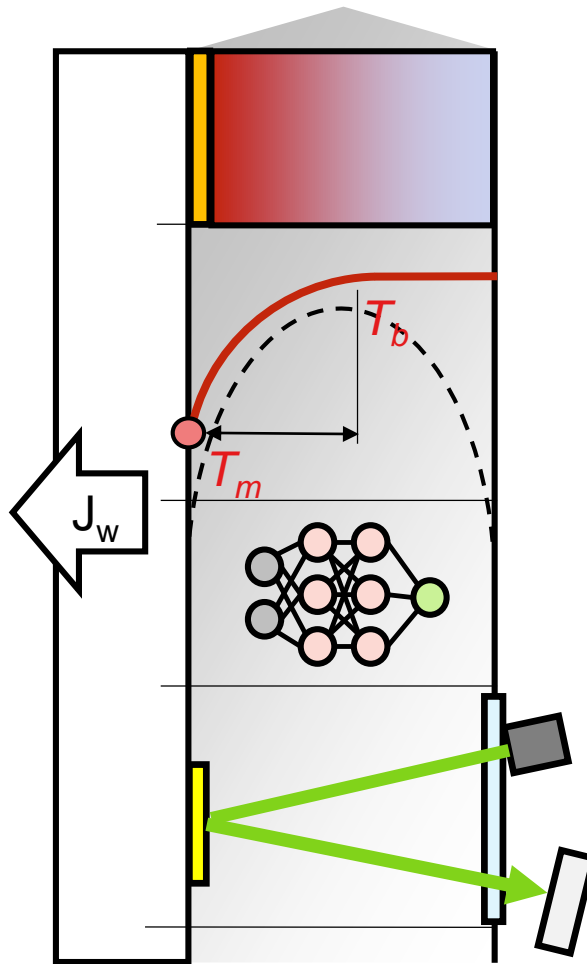
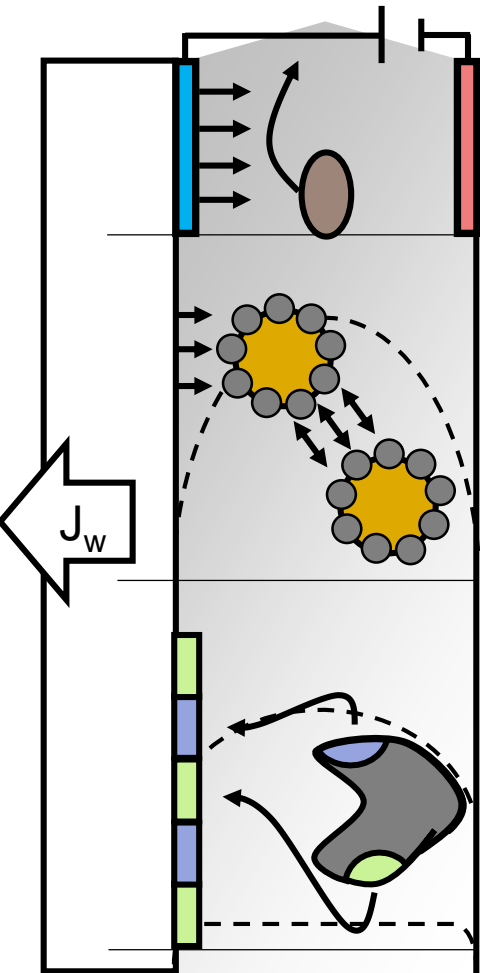
*Enhances heat/mass transfer rates by as much as 5x  
Nusselt correlations can be used for large scale module analysis*



Development of next-gen water treatment process requires combination of experiments, direct characterization, and models

*Mass and heat transfer*

*Foulant adsorption*



***Skillsets***

- Material synthesis
- Material characterization
- Experimental hardware/software design
- Fundamental modeling
- Process modeling

***LBNL***

- Advanced light source
- Molecular foundry
- Super computing at NERSC

***ESDR Division***

- Synthesis of advanced materials
- Processes for distributed water treatment
- On-line characterization of water

# Acknowledgements

*Mentor:*

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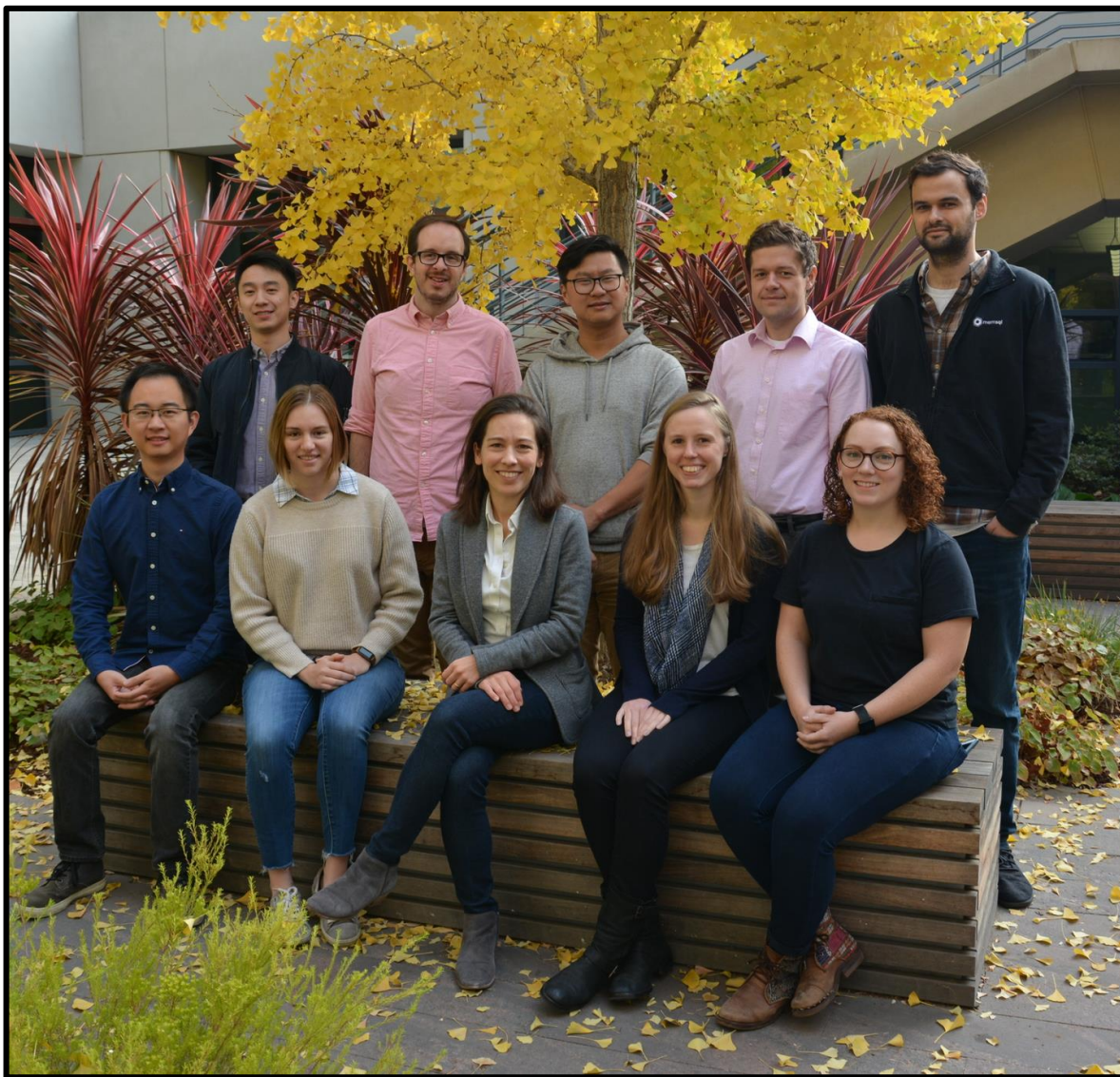


NSF: SusChEM - 1507850

NSF: CBET - 1554117



DOE: SunSHOT



# Questions?